

# SELECTIVE RECOVERY OF LITHIUM USING MEMBRANE TECHNOLOGY

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**ALTA 2019**

24<sup>th</sup> Annual Event

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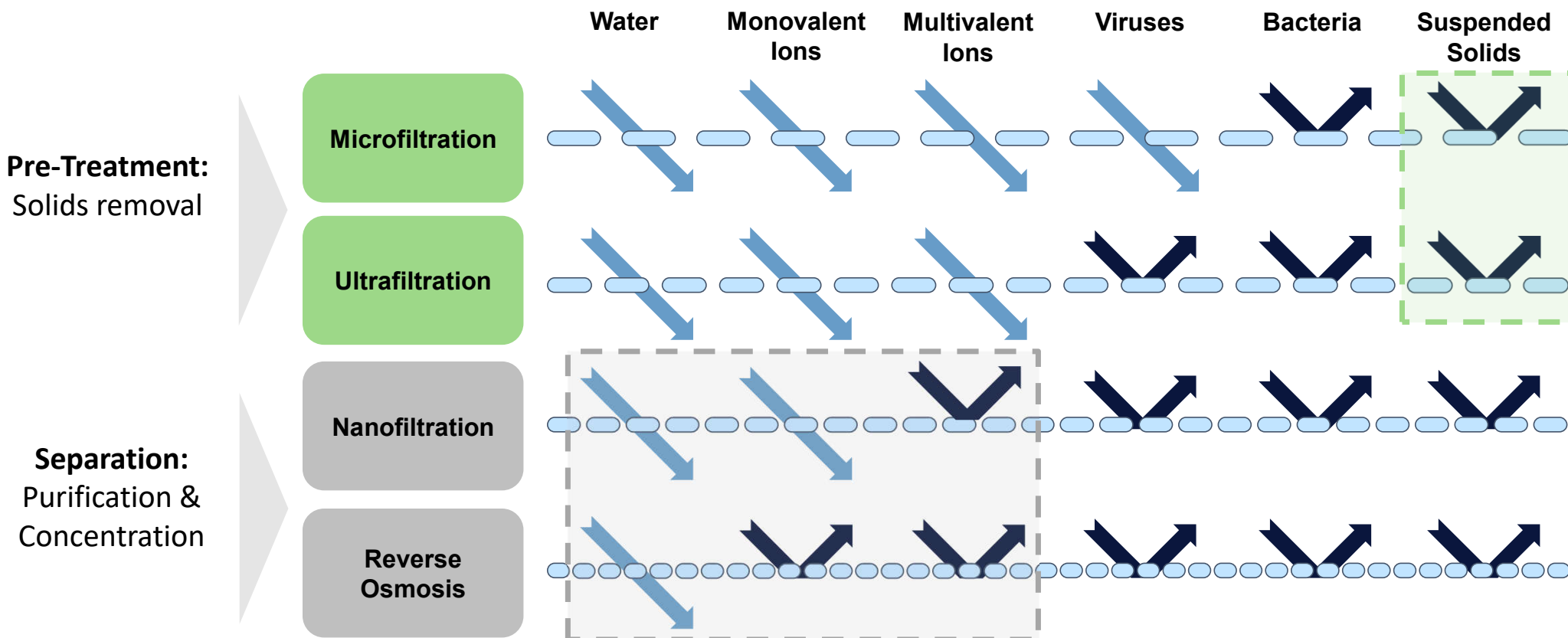
Implementation of membranes for separation,  
purification and concentration of lithium

# INTRODUCTION



# MEMBRANE REJECTION

Separation of components in solution based on size and charge



# MEMBRANE SEPARATION

## Various degrees of impurity separation



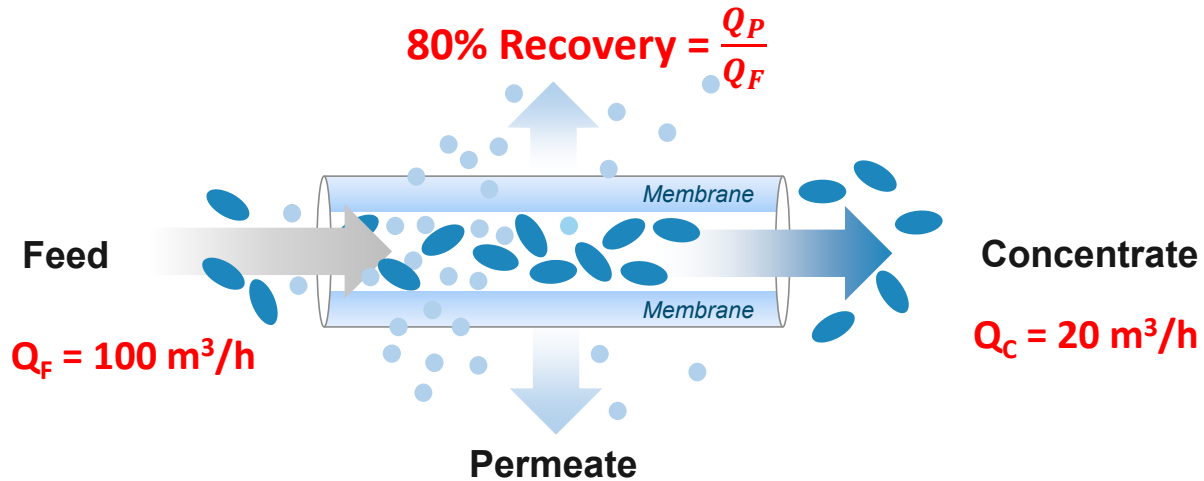
**Microfiltration**  
+  
**Ultrafiltration**  
+  
**Nanofiltration**  
+  
**Reverse Osmosis**



# MEMBRANE PROCESS

## Volumetric stream split and concentration

Copper / Cobalt electrolyte

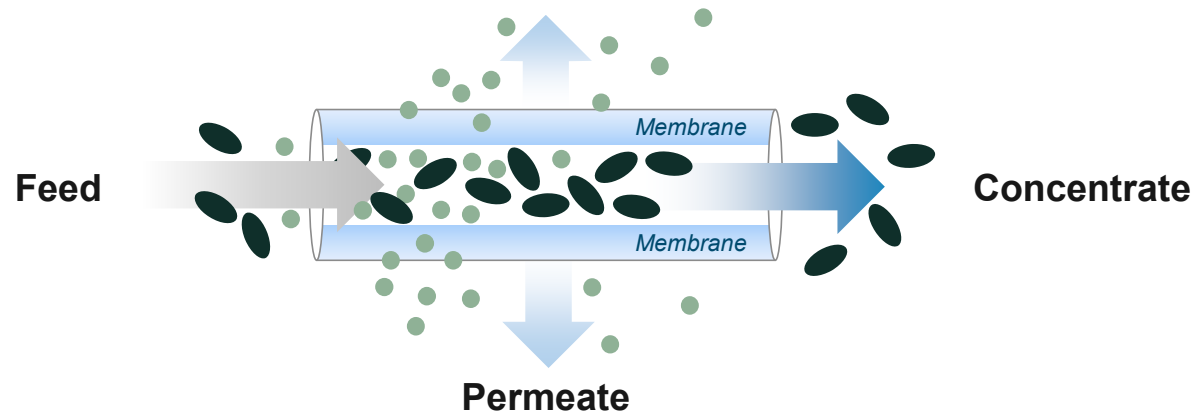


- Monovalent ions –  $\text{H}^+$ ,  $\text{Na}^+$ ,  $\text{Cl}^-$ ,  $\text{Li}^+$ ...
- Multivalent ions –  $\text{Mg}^{2+}$ ,  $\text{Fe}^{2+/3+}$ ,  $\text{Ca}^{2+}$ ...

# MEMBRANE PROCESSES IN MINING

## Nickel tailings pond water

Nickel sulphate

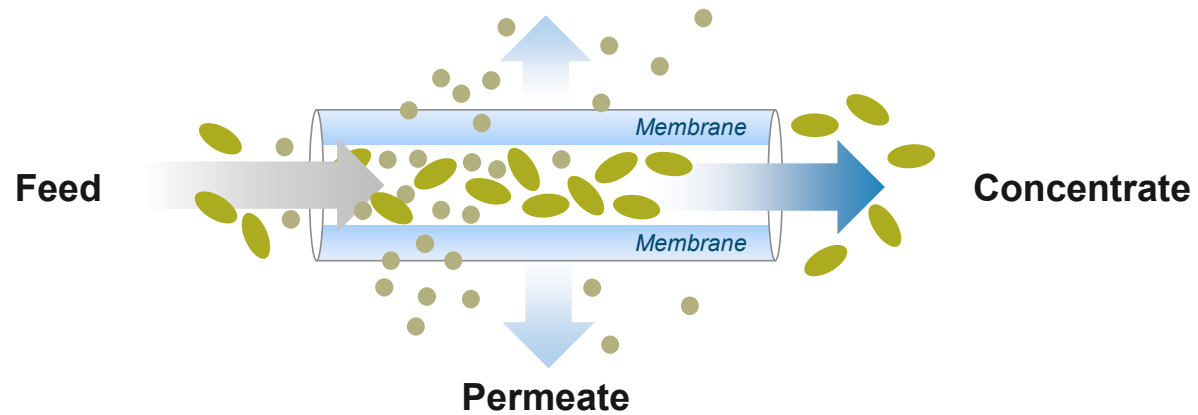


- **Monovalent ions** –  $H^+$ ,  $Na^+$ ,  $Cl^-$ ,  $Li^+$ ...
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# MEMBRANE PROCESSES IN MINING

## Concentrated uranium eluate stream

Uranium

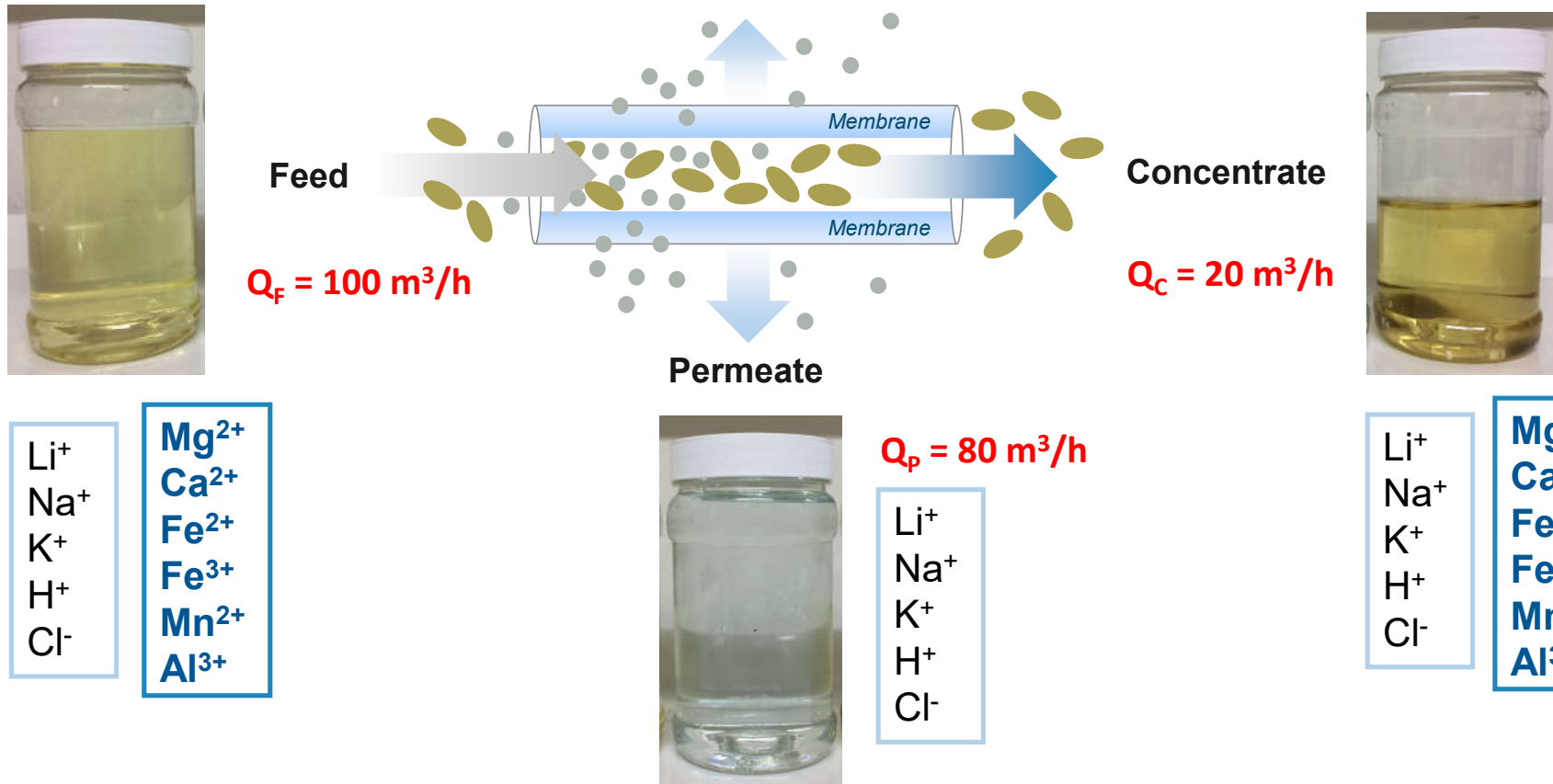


- **Monovalent ions** –  $H^+$ ,  $Na^+$ ,  $Cl^-$ ,  $Li^+$ ...
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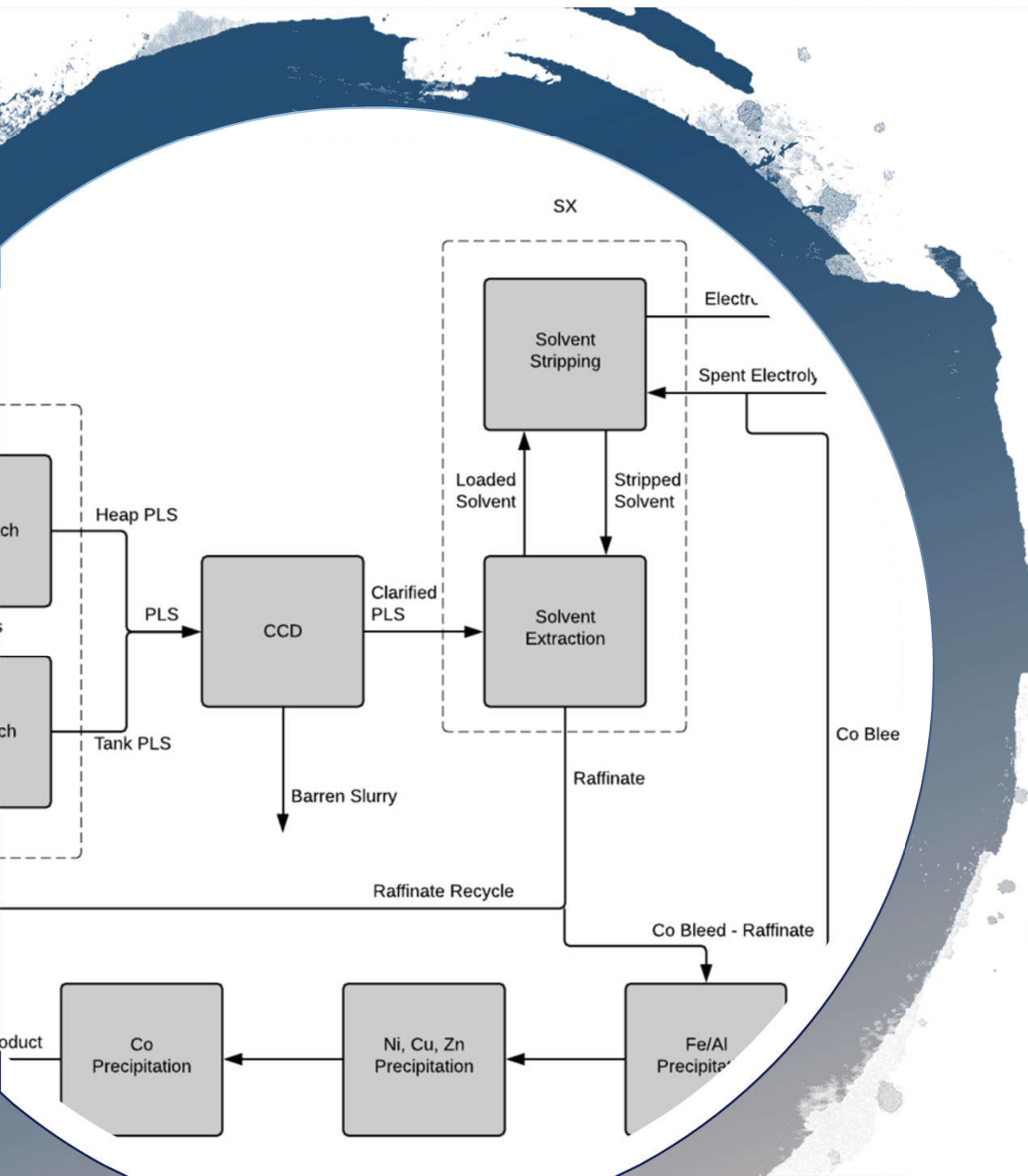
# MEMBRANE PROCESSES IN MINING

## Lithium separation from impurities

Lithium







Unit processes for membrane systems used in both lithium brine and hard-rock ore processing

# SYSTEM DESIGN AND STUDIES

# MEMBRANE SYSTEM DESIGN

## Design considerations

- High solids content
- High acidity, salinity, TDS
- Large volumes
- High concentration of impurities
- High temperature > 40°C (hard-rock ores)

## PRETREATMENT

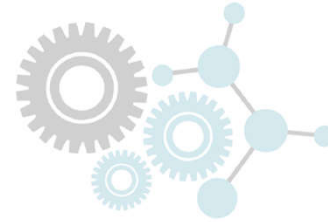
- ✓ Ceramic MF and UF membranes

## PURIFICATION

- ✓ Acid-stable NF membranes

## CONCENTRATION

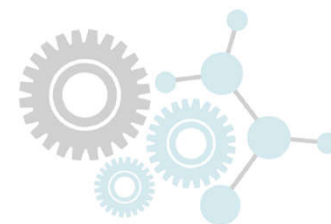
- ✓ RO / IX systems



# PRETREATMENT

## Solids removal using micro- and ultrafiltration membranes

**Li Solution:**  
Leach solution from 2 x hard-rock  
ores post solid-liquid separation

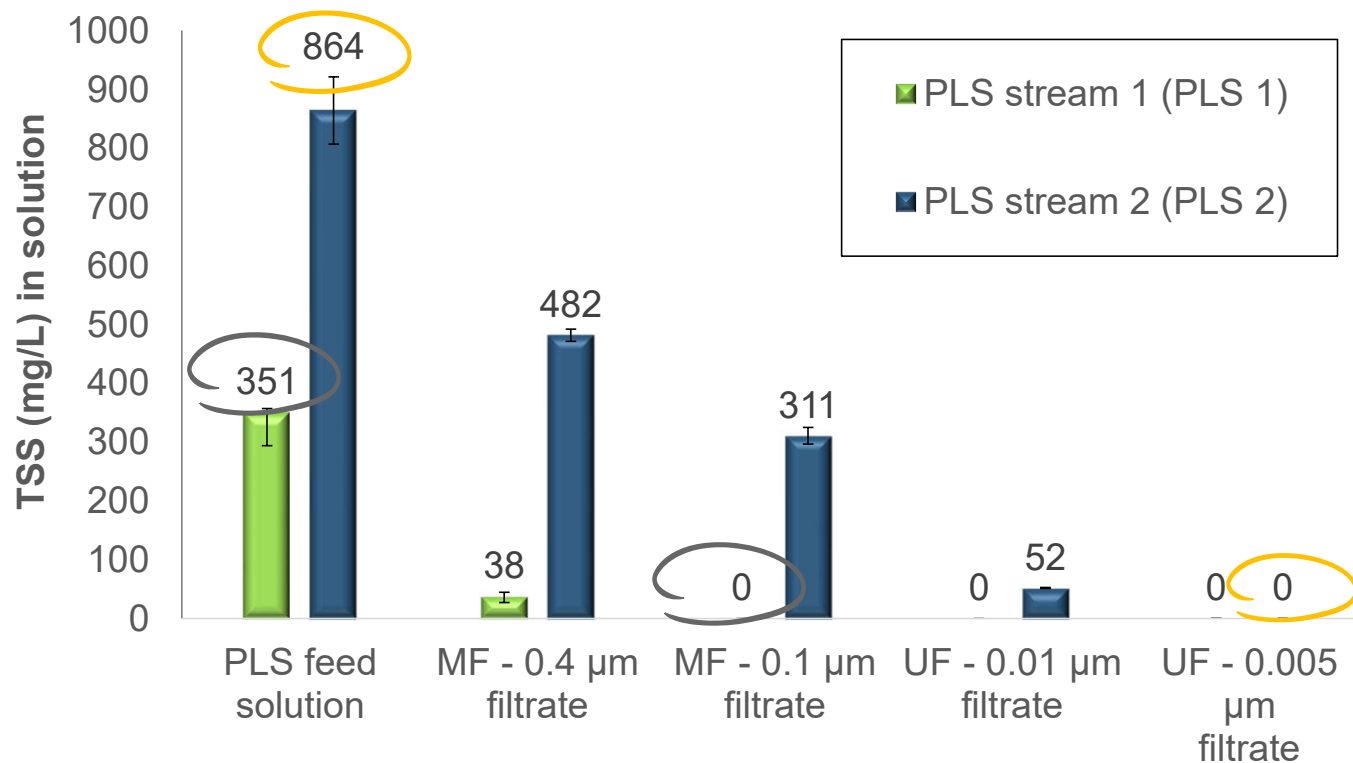


### Microfiltration

MF pore size: 0.4  $\mu\text{m}$ , 0.1  $\mu\text{m}$   
Test pressure: 3 bar  
Temperature: 28  $^{\circ}\text{C}$

### Ultrafiltration

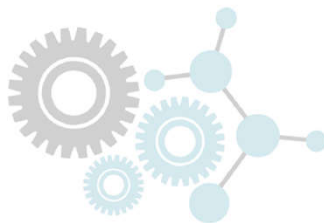
UF pore size: 0.01  $\mu\text{m}$ , 0.005  $\mu\text{m}$   
Test pressure: 12 bar  
Temperature: 28  $^{\circ}\text{C}$



# PURIFICATION

## Nanofiltration Membranes for Lithium Brine processing

**Li Solution:**  
Synthetic solution simulating  
Li brine



### Nanofiltration

Membrane: AMS A-3012  
NF pore size: 200 Da  
Test pressure: 40 bar  
Temperature: 28 °C

Global multivalent impurity rej:  
**> 98 %**

Lithium mass recovery:  
**71.4 %**

Description	Units	Case 1				Case 2				
		Feed	Perm	*Conc	Rej	Feed	Perm	*Conc	Rej	
<b>PARAMETERS</b>										
Volume	(% feed)	100	25	75	-	100	28	72	-	
pH	-	1.5	1.1	2.3	-	1.1	0.8	1.6	-	
<b>COMPONENTS</b>										
Al	(mg/L)	2 653	48	10 469	98.2%	1 917	12	6 817	99.4%	
Ca	(mg/L)	542	17	2 118	96.9%	113	2	399	98.5%	
Fe	(mg/L)	5 209	68	20 633	98.7%	3 251	42	11 502	98.7%	
K	(mg/L)	2 112	2 025	2 372	4.1%	4 315	4 177	4 670	3.2%	
Li	(mg/L)	380	375	394	1.2%	1 153	1 135	1 200	1.6%	
Mg	(mg/L)	7 230	86.8	28 660	98.8%	11 946	83.6	42 449	99.3%	
Mn	(mg/L)	206	2	817	98.8%	18	1	63	97.2%	
Na	(mg/L)	1 827	1 778	1 975	2.7%	2 819	2 726	3 058	3.3%	
H <sub>2</sub> SO <sub>4</sub> (free)	(mg/L)	18 520	17 631	21 187	4.8%	27 651	26 213	31 348	5.2%	

# PURIFICATION

## Nanofiltration Membranes for Hard-rock ore processing

**Li Solution:**  
Leach solution from Zimbabwean  
petalite ore



### Nanofiltration

Membrane: AMS A-3011  
NF pore size: 100 Da  
Test pressure: 60 bar  
Temperature: 42 °C

Global multivalent impurity rej:  
**> 99 %**

Lithium mass recovery:  
**81.7 %**

Description	Units	Case 3			
		Feed	Perm	*Conc	Rej
<b>PARAMETERS</b>					
Volume	% feed	100	15	85	-
pH	-	0.95	-	-	-
<b>COMPONENTS</b>					
Al		10.0	0.1	66.2	99.1%
Ca		145	1.2	960	99.2%
Fe		38.0	0.1	253	99.7%
K		451	431	563	4.4%
Li		5717	5494	6980	3.9%
Mg		12.0	0.0	79.7	99.6%
Na		1422	1348	1841	5.2%

# CONCENTRATION

Implementing RO membranes or IX for further processing



**Purified lithium stream now mostly contains monovalent impurities:**

- Sodium (Na<sup>+</sup>)
- Potassium (K<sup>+</sup>)

## Ion Exchange

- Already present in most Li flow sheets
- Higher efficiency in purified stream
- Better resin selectivity
- Up to 30 x Li concentration factor

## Reverse Osmosis

- Only applicable if pH 2-11
- Remove water from Li solution
- Up to 5 x Li concentration factor



# THANK YOU



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